

Sedimentation

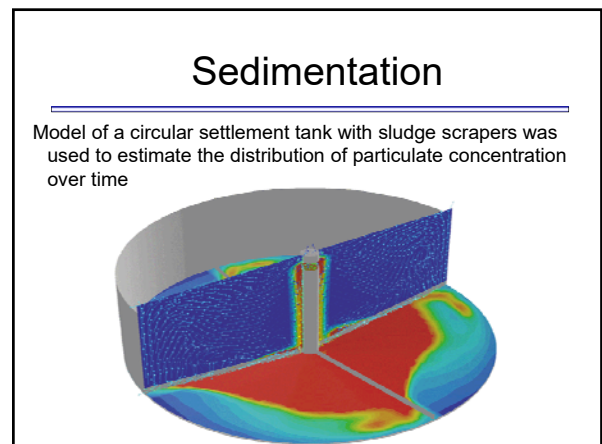
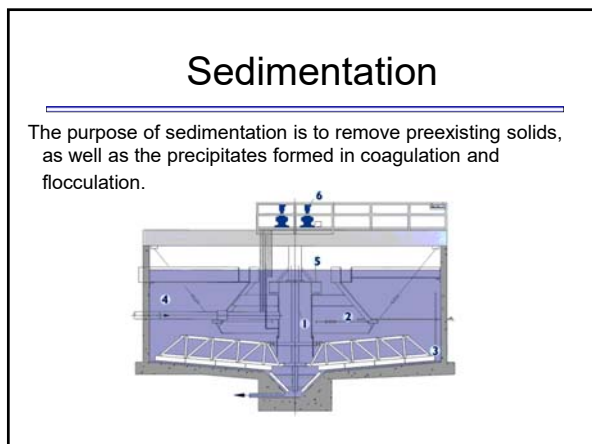
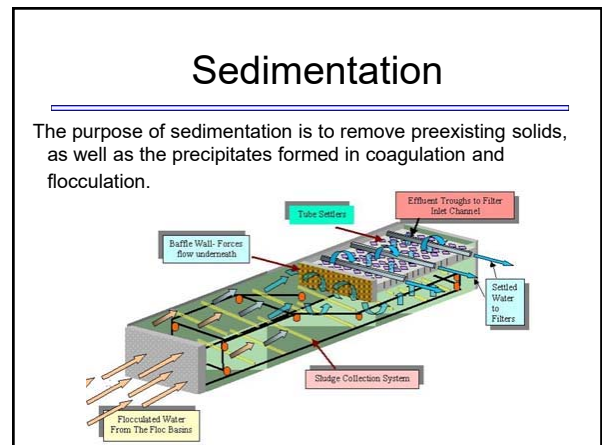
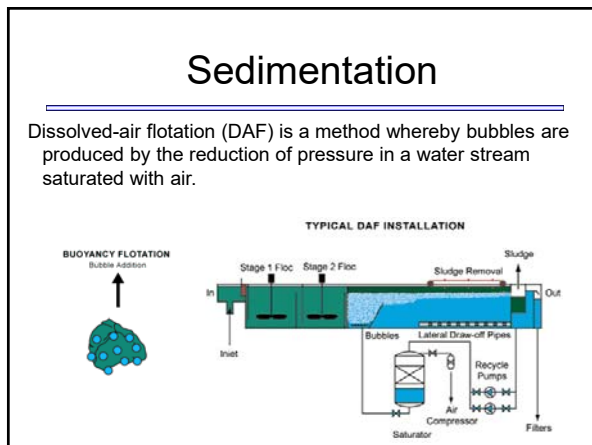
Sedimentation is the **downwards movement of an object** relative to its surrounding medium, due to the force of gravity.

Sedimentation

6144 Particles

Box dimensions: [160,120, 20]

Volume fraction: 0.13



Sedimentation



Sedimentation

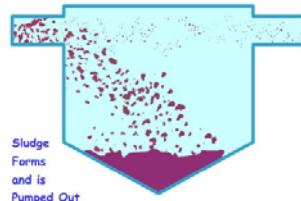


Sedimentation

Click [HERE](#) for animations about sedimentation

<http://tecalive.mtu.edu/meec/module03/WastewaterandWildlife.htm>

Sedimentation



Sedimentation

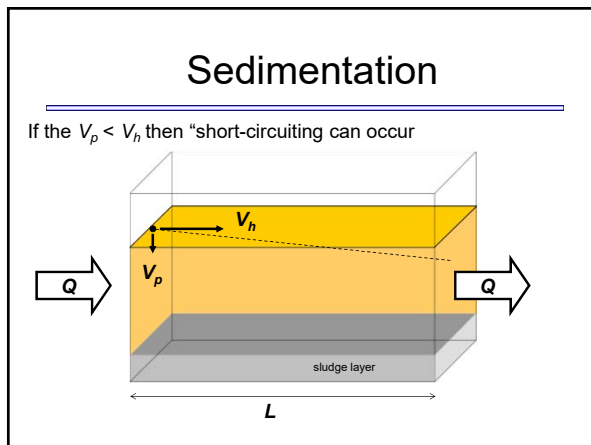
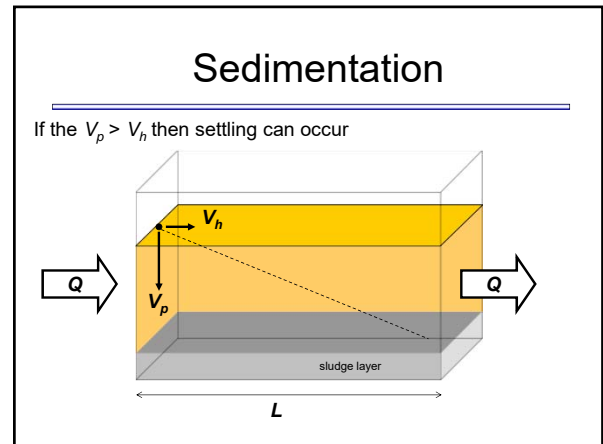
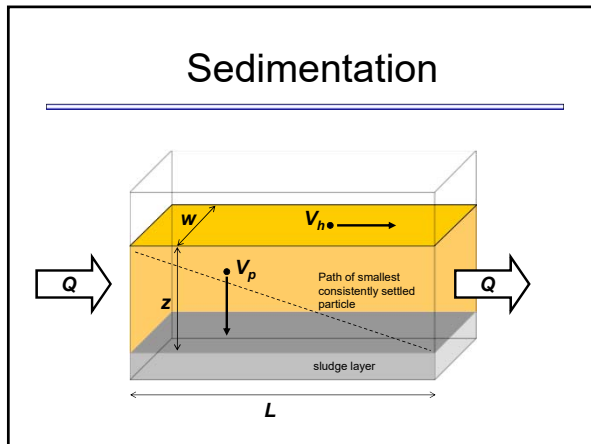
- Sedimentation is the accumulation through gravity of particulate matter at the bottom of a fluid.
- This natural process is frequently used to separate contaminants from air, water, and wastewater.
- There are four types of settling:
 - discrete
 - flocculant
 - hindered
 - compression

Sedimentation

- **Discrete** - Individual particles settle independently, neither agglomerating nor interfering with the settling of the other particles present. This occurs in water with a low concentration of particles.
- **Flocculant** - Particle concentrations are high enough that agglomeration occurs. This reduces the number of particles and increases average particle mass. The heavier particles sink faster.

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- **Hindered** - Particle concentration is sufficient that particles interfere with the settling of other particles.
- **Compression** - In the lower reaches of clarifiers where particle concentrations are highest, particles can settle only by compressing the mass of particles below.



Sedimentation

The horizontal velocity, V_h , of a particle can be approximated by considering the flowrate, Q , and the cross-sectional flow area of the tank.

$$Q = V_h A \rightarrow V_h = \frac{Q}{A}$$

$$V_h = \frac{Q}{WZ}$$

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The residence time of water in the sedimentation tank can be approximated as:

$$V_h = \frac{Q}{WZ} \rightarrow V_h \Rightarrow \frac{L}{t}$$

$$t = \frac{LWZ}{Q}$$

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Estimate of the residence time of water in a small sedimentation tank where $Q = 1$ liter/min, $L = 6$ in., $w = 6$ in., and $z = 10$ in. (dimensions of a tank in the lab).

$$t = \frac{LWZ}{Q} = \frac{6\text{ in.} \cdot (6\text{ in.}) \cdot 10\text{ in.}}{1,000\text{ ml/min}}$$

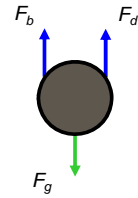
$$t = \frac{360\text{ in.}^3 \text{ min}}{1000\text{ ml}} \left[\frac{16.39\text{ ml}}{\text{in.}^3} \right] = \boxed{5.9 \text{ min}}$$

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- Discrete settling, can be analyzed by calculating the settling velocity of the individual particles contained within the water.
- The forces acting on a particle are:
 - gravity in the downward direction,
 - drag acting in the upward direction as the particle settles
 - upward buoyancy due the water displaces by the particle

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The forces acting on a settling particle are:



F_g is the force due to gravity

F_d is the drag force

F_b is the buoyant force

$$F_g = F_d + F_b$$

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The gravitational force can be expressed as:

$$F_g = m_p g$$

Using the density and volume of the particle yields:

$$F_g = \rho_p V_p g$$

where: ρ_p is the density of the particle, lb-mass/ft.³,
 V_p is the volume of the particle, ft.³, and
 g is the gravitational constant, ft./s²

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The drag on the particle can be calculated by the drag equation from fluid mechanics

$$F_d = \frac{1}{2} C_d A \rho_w v^2$$

where C_d is the drag coefficient, dimensionless,
 A is the particle cross-sectional area, ft.²,
 ρ_w is the density of water, lb-mass/ft.³,
 v is the velocity, ft./sec.

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The buoyant force acting on the particle is:

$$F_b = m_w g$$

Substituting the particle volume and density of water, yields:

$$F_b = \rho_w V_p g$$

where: ρ_w is the density of water, lb-mass/ft.³,

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By balancing the forces acting on a settling particle and using the relationships for F_g the force due to gravity, F_d the drag force, and F_b the buoyant force, the following relationship can be developed:

$$\rho_p V_p g = \frac{1}{2} C_d A \rho_w v^2 + \rho_w V_p g$$

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Solving for the settling velocity, v , results in:

$$v = \sqrt{\frac{2(\rho_p - \rho_w)V_p g}{C_d A \rho_w}}$$

If the particle is assumed to be round and the formulas for area and volume of a sphere are used:

$$v = \sqrt{\frac{4(\rho_p - \rho_w)d_p^3 g}{3C_d \rho_w}}$$

where d_p is the diameter of the particle

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At low Reynolds numbers (for $N_{Re} < 1$) C_d can be approximated by:

$$C_d = \frac{24}{N_{Re}}$$

For Reynolds Numbers in transition flow, $1 < N_{Re} < 10,000$, the drag coefficient for spheres is:

$$C_d = \frac{24}{N_{Re}} + \frac{3}{\sqrt{N_{Re}}} + 0.34$$

For turbulent flow, $N_{Re} > 10,000$, the relationship for the drag coefficient for spheres is:

$$C_d = 0.4$$

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The Reynolds Number is: $N_{Re} = \frac{\rho v d}{\mu}$

where μ is the absolute viscosity of the water, lb-force-sec./ft.² (at 50°F, $\mu = 2.73(10^{-5})$ lb.-sec./ft.²).

For $N_{Re} < 1$ the particle settling velocity can be estimated as a function of the properties of the particle and water, and the particle diameter, or

$$v_p = \frac{(\rho_p - \rho_w)d^2 g}{18\mu}$$

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This relationship is known as Stokes' law, and the velocity is known as the Stokes velocity.

$$v_p = \frac{(\rho_p - \rho_w)d^2 g}{18\mu}$$

The vertical velocity of water in a settling basin is often described as the **overflow rate (OFR)**.

It is usually expressed as gal./ft.²-day (m³/m²-day).

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The overflow rate is calculated in the following way:

$$OFR = \frac{Q}{A}$$

where: **OFR** is the overflow rate, gal./ft.²-day,
Q is the flowrate, gal./day, and
A is the clarifier area, ft.².



Treatment Processes



Any Questions?

